

Preparation of $\text{LiZnPO}_4 \cdot \text{H}_2\text{O}$ via a novel modified method and its non-isothermal kinetics and thermodynamics of thermal decomposition

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Abstract The single phase $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ was directly synthesized via solid-state reaction at room temperature using $\text{LiH}_2\text{PO}_4 \cdot \text{H}_2\text{O}$, $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$, and Na_2CO_3 as raw materials. XRD analysis showed that $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ was a compound with orthorhombic structure. The thermal process of $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ experienced two steps, which involved the dehydration of one crystal water molecule at first, and then the crystallization of LiZnPO_4 . The DTA curve had the one endothermic peak and one exothermic peak, respectively, corresponding to dehydration of $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ and crystallization of LiZnPO_4 . Based on the iterative iso-conversional procedure, the average values of the activation energies associated with the thermal dehydration of $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$, was determined to be $86.59 \text{ kJ mol}^{-1}$. Dehydration of the crystal water molecule of $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ is single-step reaction mechanism. A method of multiple rate iso-temperature was used to define the most probable mechanism $g(\alpha)$ of the dehydration step. The dehydration step is contracting cylinder model ($g(\alpha) = 1 - (1 - \alpha)^{1/2}$) and is controlled by phase boundary reaction mechanism. The pre-exponential factor A was obtained on the basis of E_a and $g(\alpha)$. Besides, the thermodynamic parameters (ΔS^\ddagger , ΔH^\ddagger , and ΔG^\ddagger) of the dehydration reaction of $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ were determined.

Keywords $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ · Non-isothermal kinetics · Thermodynamics · Thermal decomposition · Solid-state reaction at room temperature

Introduction

The synthesis and structural characterization of zinc phosphates have received considerable amount of attention because of their potential applications as new materials that may have ion exchange, absorption, separation, ionic conductivity, and heterogeneous catalytic properties [1–9].

A water-containing lithium zinc phosphate, $\text{LiZnPO}_4 \cdot \text{H}_2\text{O}$ [5, 6], was described having a zeolite type ABW structure, i.e., isomorphous with zeolite Li-A(BW), $\text{LiAlSiO}_4 \cdot \text{H}_2\text{O}$. Hydrothermal techniques have been used for the preparation of the $\text{LiZnPO}_4 \cdot \text{H}_2\text{O}$ [5, 6].

Solid-state reaction at room temperature or near room temperature was a novel synthetic technique which has been developed in recent decade [10–23]. Recently, we successfully used this novel technique to synthesize $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ with $\text{LiH}_2\text{PO}_4 \cdot \text{H}_2\text{O}$, and ZnCO_3 as raw materials [22].

Wu and Jiang [23] prepared ZnCO_3 via solid-state reaction at room temperature with $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$ and NH_4HCO_3 as raw materials. Therefore, it suggested that the $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ can be directly synthesized via the modified method using $\text{LiH}_2\text{PO}_4 \cdot \text{H}_2\text{O}$, $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$, and Na_2CO_3 as raw materials.

So, as a part of the system research, the aim of this study was to prepare single phase $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ via the above method with $\text{LiH}_2\text{PO}_4 \cdot \text{H}_2\text{O}$, $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$, and Na_2CO_3 and to study the kinetics and thermodynamics of the decomposition of $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ using TG-DTA technique. Non-isothermal kinetics of the decomposition process of $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ was interpreted by a modified method [24–29], the apparent activation energy E_a was obtained from iterative procedure [29], the most probable mechanism function $g(\alpha)$ of the thermal decomposition reaction was deduced from multiple rate iso-temperature

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method, pre-exponential factor A was calculated on the basis of E_a and $g(\alpha)$ subsequently. The kinetic (E_a , A , mechanism) and thermodynamic parameters (ΔH^\ddagger , ΔS^\ddagger , ΔG^\ddagger) of the dehydration reaction of α -LiZnPO₄·H₂O were discussed for the first time.

Experiment

Reagent and apparatus

All chemicals were of reagent grade purity. TG/DTA measurements were made using a Netsch 40PC thermogravimetric analyzer. Samples of 50 mg mass were used for the experiments varied out at heating rates of 5, 10, 15, 20 °C min⁻¹ up to 800 °C. Pure gas was argon gas of high purity, flowing at 20 mL min⁻¹. The samples were loaded without pressing into an alumina crucible, α -alumina calcined up to 1373 K was used as a standard reference material. (The results presented in the article were calculated by the programs compiled by ourselves).

X-ray powder diffraction (XRD) was performed at a scanning rate of 5° min⁻¹ from 5° to 65° for 2θ at room temperature using a Rigaku D/max 2500 V diffractometer equipped with a graphite monochromator and a Cu target. Fourier transform infrared (FTIR) spectroscopy using a Nicolet NEXUS-470 spectrometer in the wavenumbers range of 400–4000 cm⁻¹. The FTIR spectra were taken on KBr pellets. The morphology of the product and its calcined samples were examined by S-3400 scanning electron microscopy (SEM). The samples were mounted on an aluminum slice then coated with Au.

Preparation of α -LiZnPO₄·H₂O

The lithium zinc phosphate hydrate α -LiZnPO₄·H₂O was prepared by solid-state reaction at room temperature using LiH₂PO₄·H₂O, ZnSO₄·7H₂O, and Na₂CO₃ as starting materials. In a typical synthesis: first, LiH₂PO₄·H₂O (31.5 mmol, 3.84 g), ZnSO₄·7H₂O (30.0 mmol, 8.64 g), and surfactant polyethylene glycol-400 (PEG-400) (1.5 mL) were put in a mortar, and ground to form uniform mixture. Then after powder of Na₂CO₃ (30.0 mmol, 3.18 g) was added into the mixture, and the mixture was fully ground for 30 min. The reactant mixture gradually became damp, and then a paste formed quickly. The reaction mixture was kept at room temperature for 4 h. The mixture was washed with deionized water to remove soluble inorganic salts until SO₄²⁻ ion could not be visually detected with a 0.5 mol L⁻¹ BaCl₂ solution. The solid was then washed with a small amount of anhydrous ethanol and dried at 80 °C for 3 h to give the single phase α -LiZnPO₄·H₂O.

Method of determining kinetic parameters, model function, and thermodynamic parameters

Theoretical

Kinetic equation of solid-state reaction can be expressed as Eq. 1:

$$\frac{d\alpha}{dt} = A \exp\left(-\frac{E_a}{RT}\right) f(\alpha) \quad (1)$$

When heating rate is kept constant, that is: $q = dT/dt$. Equation 1 can be rewritten into the Eq. 2:

$$\frac{d\alpha}{dT} = \frac{A}{q} \exp\left(-\frac{E_a}{RT}\right) f(\alpha) \quad (2)$$

Rearranging Eq. 2, one obtains:

$$\frac{d\alpha}{f(\alpha)} = \frac{A}{q} \exp\left(-\frac{E_a}{RT}\right) dT \quad (3)$$

where E_a is apparent activation energy, q is the heating rate (5, 10, 15, 20 °C min⁻¹), A is pre-exponential factor, R is the gas constant, α is called conversion degree.

Calculation of activation energy by iterative procedure

From Eq. 3, OFW equation [30–32] and KAS [33, 34] equation are deduced.

OFW equation:

$$\ln q = \ln \frac{0.0048AE_a}{g(\alpha)R} - 1.0516 \frac{E_a}{RT} \quad (4)$$

KAS equation:

$$\ln \frac{q}{T^2} = \ln \frac{AR}{g(\alpha)E_a} - \frac{E_a}{RT} \quad (5)$$

The iterative procedure [26–28, 35] is used to calculate the approximate value of E_a approach to the exact value, the Equations are expressed:

$$\ln \frac{q}{H(x)} = \ln \frac{0.0048AE_a}{g(\alpha)R} - 1.0516 \frac{E_a}{RT} \quad (6)$$

and

$$\ln \frac{q}{h(x)T^2} = \ln \frac{AR}{g(\alpha)E_a} - \frac{E_a}{RT} \quad (7)$$

Because

$$g(\alpha) = \int_0^\alpha \frac{d\alpha}{f(\alpha)} \approx \frac{A}{q} \int_0^T e^{-E_a/RT} dT = \frac{AE_a e^{-x}}{qR x^2} h(x) \quad (8)$$

and where $h(x)$ is expressed by the fourth Senum and Yang approximation formulae [28, 36]:

$$h(x) = \frac{x^4 + 18x^3 + 86x^2 + 96x}{x^4 + 20x^3 + 120x^2 + 240x + 120} \quad (9)$$

where $x = E_a/RT$ and $H(x)$ is equal to:

$$H(x) = \frac{\exp(-x)h(x)/x^2}{0.0048 \exp(-1.0516x)} \quad (10)$$

The iterative procedure performed involved the following steps [25, 26]: (i) Assume $h(x) = 1$ or $H(x) = 1$ to estimate the initial value of the activation energy E_{a1} . The conventional iso-conversional methods stop the calculation at this step; (ii) using E_{a1} , calculate a new value of E_{a2} for the activation energy from the plot of $\ln[q/H(x)]$ versus $1/T$ or $\ln[q/h(x)T^2]$ versus $1/T$; (iii) repeat step (ii), replacing E_{a1} with E_{a2} . When $E_{ai} - E_{a(i-1)} < 0.01 \text{ kJ mol}^{-1}$, the last value of E_{ai} was considered to be the exact value of the activation energy of the reaction. These plots are model independent since the estimation of the apparent activation energy does not require selection of particular kinetic model (type of $g(\alpha)$ function). Therefore, the activation energy values obtained by this method are usually regarded as more reliable than these obtained by a single TG curve.

Determination of the most probably mechanism function

The following equation is used to estimate the most correct reaction mechanism, i.e., $g(\alpha)$ function [26]:

$$\ln g(\alpha) = \left[\ln \frac{AE_a}{R} + \ln \frac{e^{-x}}{x^2} + \ln h(x) \right] - \ln q \quad (11)$$

The conversions α corresponding multiple rates at the same temperature are put into the left of Eq. 11, combined with thirty-one types of mechanism functions [26], the slope k and correlation coefficient r are obtained from the plot of $\ln[g(\alpha)]$ versus $\ln q$. The probable mechanism function is that for which the value of the slope k is near to -1.00000 and correlation coefficient r is better. If several $g(\alpha)$ answer for this requirement, the conversions α corresponding to multiple rates at several the same temperatures are applied to calculate the probable mechanism by the same method, the most probable mechanism function is that for which among the results of k and r , the value of k is closest to -1.00000 and the correlation coefficient is higher.

Calculation of pre-exponential factor A

The pre-exponential factor A can be estimated from the intercept of the plots of Eqs. 6 and 7, inserting the most probable $g(\alpha)$ function determined [25].

Calculation of thermodynamic parameters of thermal decomposition reaction [37, 38]

The change of the entropy (ΔS^\ddagger) may be calculated according to the Eq. 12:

$$\Delta S^\ddagger = R \ln \left(\frac{Ah}{e\chi k_B T_P} \right) \quad (12)$$

where A is the pre-exponential factor, $e = 2.7183$ is the Neper number, χ is the transition factor, which is unity for monomolecular reactions, k_B is the Boltzmann constant ($1.381 \times 10^{-23} \text{ J K}^{-1}$), h is the Plank constant ($6.626 \times 10^{-34} \text{ J s}$); T_P is the peak temperature in DTG curve, R is the gas constant ($8.314 \text{ J mol}^{-1} \text{ K}^{-1}$).

The change of the enthalpy (ΔH^\ddagger) may be obtained according to the Eq. 13:

$$\Delta H^\ddagger = E^\ddagger - RT_P \quad (13)$$

where E^\ddagger is the activation energy, E_a , obtained from the iterative procedure of KAS method.

The change of Gibbs free energy ΔG^\ddagger for the decomposition reaction can be calculated using the well-known thermodynamic Eq. 14:

$$\Delta G^\ddagger = \Delta H^\ddagger - T_P \Delta S^\ddagger \quad (14)$$

Results and discussion

XRD analysis of the product and its calcined samples

Figure 1 shows the XRD patterns of the product dried at 80 °C and the product resulting from calcination at 650 °C for 2 h.

From Fig. 1a, the results show that all diffraction peaks in the pattern could be indexed to obtain lattice parameters: $a = 10.52716(7) \text{ \AA}$, $b = 8.11728(6) \text{ \AA}$, and $c = 5.02327(5) \text{ \AA}$; $\alpha = \beta = \gamma = 90^\circ$ that are in agreement with that of orthorhombic LiZnPO₄·H₂O, with space group Pna21(33) and cell parameters: $a = 10.575 \text{ \AA}$, $b = 8.076 \text{ \AA}$, and $c = 4.994 \text{ \AA}$, and $\alpha = \beta = \gamma = 90^\circ$, from PDF card 83-0263. No diffraction peaks of other impurities, such as Zn₃(PO₄)₂·4H₂O and NaZnPO₄·H₂O, are observed, which indicates that the single phase α -LiZnPO₄·H₂O [5] is synthesized by solid-state reaction at room temperature. It is obvious that the synthesis described here is a modified one and also more convenient one when compared with that reported by us [22]. From Fig. 1b, all the diffraction peaks in the XRD pattern are found to be in agreement with that of monoclinic LiZnPO₄, space group Cc (9), from PDF card 79-0804.

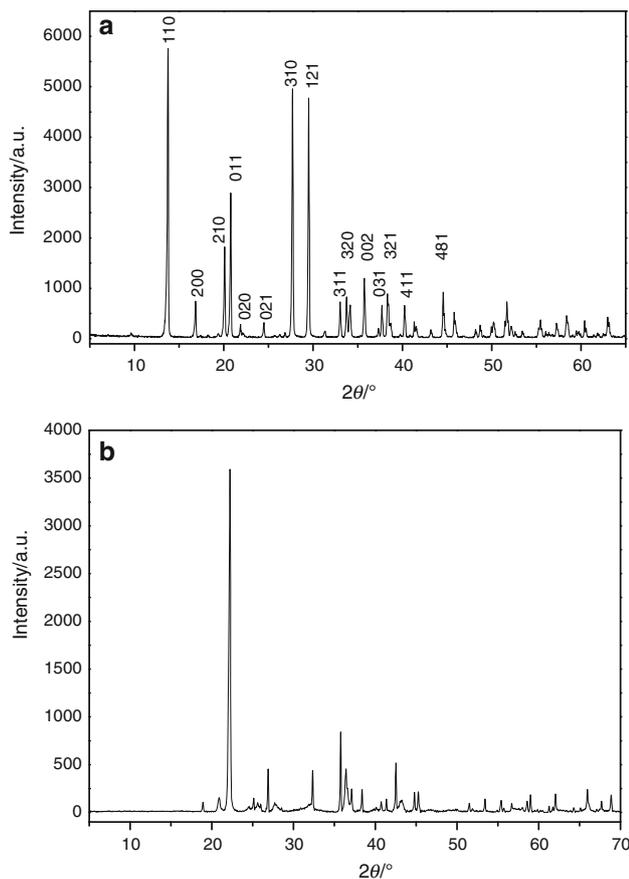


Fig. 1 XRD patterns of the product (a) and its calcined product (b) at 650 °C for 2 h

TG/DTA analysis of the synthetic product

Figure 2 shows the TG/DTA curves of the synthetic product at four different heating rates from ambient temperature to 800 °C, respectively.

The TG curves show that thermal decomposition of the α -LiZnPO₄·H₂O below 800 °C occurs in one well-defined step. The mass loss starts at about 120 °C, ends at about 270 °C, and characterized by a strong endothermic DTA peak at about 200 °C that can be attributed to dehydration from α -LiZnPO₄·H₂O and the formation of LiZnPO₄. The observed mass loss in the TG curve is 9.71%, which is in good agreement with 9.72% theoretic mass loss of one water molecule eliminated from α -LiZnPO₄·H₂O. The exothermic DTA peak at about 545 °C can be attributed to the phase change from amorphous LiZnPO₄ to monoclinic LiZnPO₄.

IR spectroscopic analysis of the product and its calcined samples

FT-IR spectra of the prepared and its calcined samples are shown in Fig. 3. From Fig. 3a, the strong band of the prepared sample at 1064 cm⁻¹ is attributed to the O-P

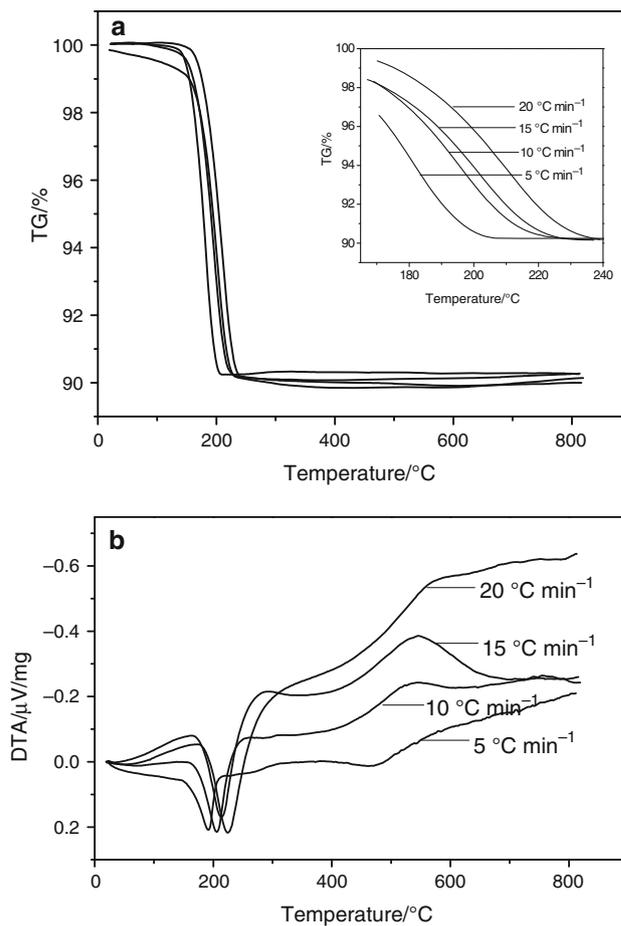


Fig. 2 TG/DTA curves of the LiZnPO₄·H₂O at different heating rates

tetrahedron vibration. The bending OPO vibrations appear in the region of 500–627 cm⁻¹. The strong and broad band around 3000–3600 cm⁻¹ is assigned to the stretching OH vibration of the water molecule, while the band observed at 1607 cm⁻¹ is assigned to the bending mode of the HOH. It can be seen from Fig. 3b that the intensity of bands at 2300–3600 and 1607 cm⁻¹ disappear after calcination. It is explained by the fact that α -LiZnPO₄·H₂O finish elimination of its crystal water after calcination.

SEM analysis of the synthetic product and its calcined samples

The morphology of α -LiZnPO₄·H₂O and its calcined sample are shown in Fig. 4. From Fig. 4a, it can be seen that the α -LiZnPO₄·H₂O sample is composed of prisms. Figure 4b shows the SEM micrographs of samples obtained at 650 °C. It can be seen that the morphology of the sample has been become block-like shapes, and there is soft agglomeration phenomenon among one particle of sample.

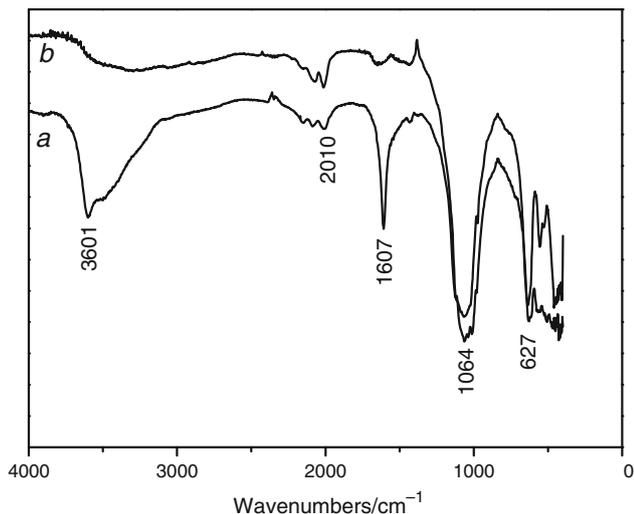


Fig. 3 The infrared spectroscopy of the product (a) and its calcined product (b) at 650 °C for 2 h

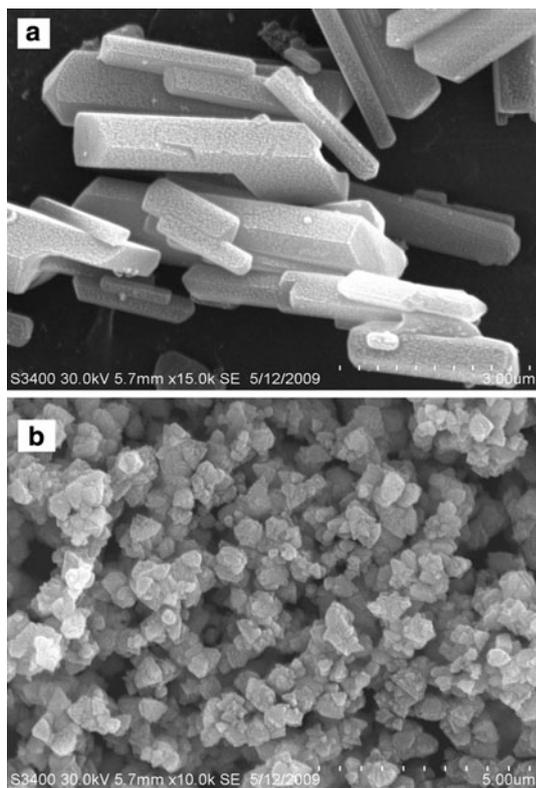


Fig. 4 SEM image of the product (a) and its calcined product (b) at 650 °C for 2 h

Thermal decomposition kinetics

In accordance with TG/DTA analysis and XRD analysis of the synthetic product, and its calcined product mentioned above, thermal process of $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ below

Table 1 Temperatures corresponding to conversion degrees at various heating rates

Conversion degree/a	Heating rate/°C min ⁻¹			
	T/K			
	5	10	15	20
0.2	434.78	445.11	444.10	458.40
0.3	440.79	452.39	453.70	465.84
0.4	445.62	458.15	460.76	471.91
0.5	449.97	463.23	467.66	476.55
0.6	453.87	468.03	472.66	481.36
0.7	457.81	472.67	477.54	486.12
0.8	462.06	477.31	482.76	491.13

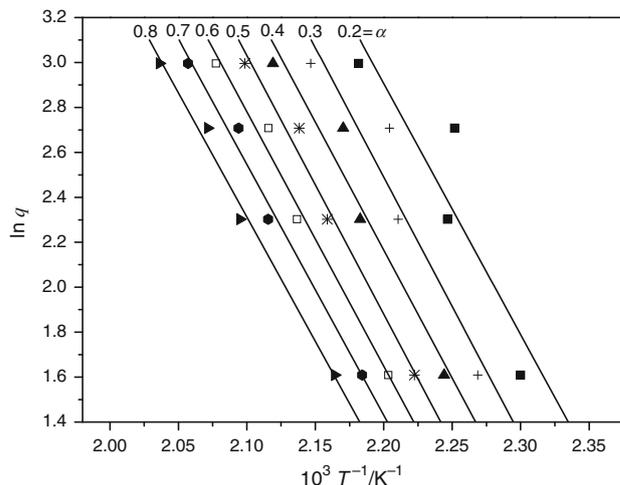
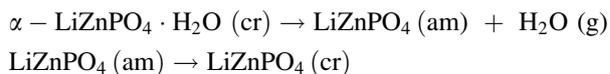


Fig. 5 Isoconversional plots at various conversion degrees for $\text{LiZnPO}_4 \cdot \text{H}_2\text{O}$ draw according OFW calculation procedure

800 °C consists of two steps, which can be expressed as follows:



Above two steps involve the dehydration of one crystal water molecule at first, and then the crystallization of LiZnPO_4 . The dehydration step will be studied using non-isothermal method in this article.

According to the non-isothermal method, the basic data of α and T collected from the TG curves of the thermal decomposition of $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ at various heating rates (5, 10, 15, and 20 °C min⁻¹) are illustrated in Table 1.

Calculation of activation energy E_a by iterative procedure

According to Eqs. 4 and 5, the iso-conversional calculation procedures of OFW and KAS were used. The corresponding

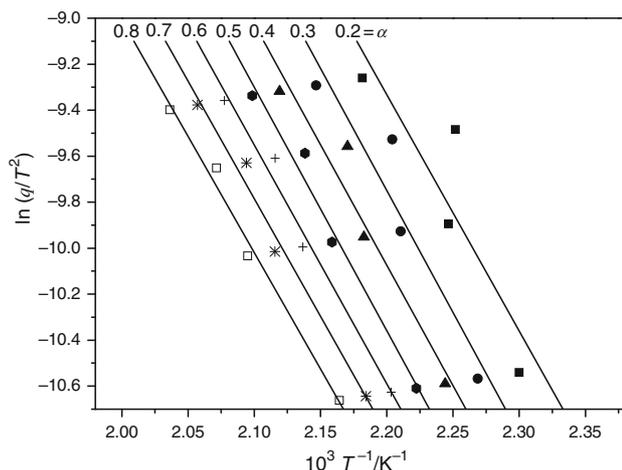


Fig. 6 Isoconversional plots at various conversion degrees for $\text{LiZnPO}_4 \cdot \text{H}_2\text{O}$ draw according KAS calculation procedure

OFW lines and KAS lines obtained at different conversion degrees α and different heating rates q are shown in Figs. 5 and 6, respectively.

The values of E_a of the dehydration of $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ corresponding to different conversions α are obtained by the OFW and KAS calculation procedure and the above iterative method, and shown in Table 2.

As shown in Table 2, compared with the values of E_a obtained by iterative method and OFW or KAS method, that obtained by OFW method is general higher (excessing about $2.57\text{--}3.09 \text{ kJ mol}^{-1}$), however, the results obtained by iterative method and KAS method are very close to each other (differing about 0.28 kJ mol^{-1}). Meanwhile, it can be discovered that the values obtained from the plot of $\ln[q/H(x)]$ versus $1/T$ or $\ln[q/(h(x)T^2)]$ versus $1/T$ by iterative procedure are very close to each other. It is obvious that the values of E_a obtained from iterative method or KAS method are more reliable, so the suggestion that the

values obtained from the two methods determined the range of E_a is reasonable, while the heating rates are $5, 10, 15, 20 \text{ }^\circ\text{C min}^{-1}$, the value of E_a is equal to $86.59 \text{ kJ mol}^{-1}$ at $0.20 < \alpha < 0.80$. From Table 2, it is seen activation energies at different conversion degree, varies here by only about 2.1%, indicating that a single-step kinetic process takes place in thermal dehydration reaction.

Determination of the most probably mechanism function

Determination of the most probably mechanism function by multiple rate iso-temperature method roughly

The conversions for $q = 5, 10, 15, 20 \text{ }^\circ\text{C min}^{-1}$ at the same temperature are illustrated in Table 3. An appropriate temperature is randomly selected; the range of the conversions of this temperature should be within 0.10–0.90. We choose the corresponding conversions of $T = 454 \text{ K}$ for example to put into thirty-one types of mechanism functions [26]. The slope k , correlation coefficient r , and intercept B of linear regression of $\ln[g(\alpha)]$ versus $\ln q$ are obtained. The results of the linear regression show that the slopes of No. 13 and 14 mechanism function are closer to -1.00000 than others and with better correlation coefficient r , but which type of mechanism is the most probable one, it needs further research.

Determination of the most probably mechanism function by multiple rate iso-temperature method precisely

We randomly choose several temperatures (Table 3) which corresponding conversions $0.1 < \alpha < 0.9$ to calculate the slope k , correlation coefficient r , and intercept B of No. 13 and 14 mechanism function by the same method. The

Table 2 The activation energies for thermal decomposition of $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$, E_a (kJ mol^{-1}), and the intercept, B , at different conversion degree and calculating procedure

Conversion degree/ α	$E_a/\text{kJ mol}^{-1}$				B	
	OFW method	KAS method	$\ln[q/H(x)] \sim 1/T$	$\ln[q/(h(x)T^2)] \sim 1/T$	Eq. 6	Eq. 7
0.2	88.33	85.46	85.73	85.73	26.57440	13.43152
0.3	91.04	88.21	88.47	88.47	26.94590	13.73985
0.4	90.07	87.09	87.37	87.37	26.30391	13.12306
0.5	91.02	88.02	88.30	88.30	26.28595	13.08382
0.6	89.46	86.32	86.60	86.60	25.56902	12.40566
0.7	88.29	85.02	85.31	85.31	24.97933	11.84614
0.8	87.45	84.06	84.36	84.36	24.48286	11.37209
Average	89.38	86.31	86.59	86.59		

$\ln[q/H(x)] \sim 1/T$ is the iterative results of OFW method and $\ln[q/(h(x)T^2)] \sim 1/T$ is the iterative results of KAS method, respectively B is the intercept of the plots of Eqs. 6 and 7

Table 3 The relation of temperature and conversion α at different heating rates q ($^\circ\text{C min}^{-1}$)

T/K	α			
	$q = 5$	$q = 10$	$q = 15$	$q = 20$
451	0.52616	0.27798	0.26789	0.12126
452	0.55259	0.29344	0.27914	0.13067
453	0.57822	0.30946	0.29128	0.14062
454	0.60379	0.32602	0.30388	0.15091
455	0.62924	0.34309	0.31644	0.16129
456	0.65529	0.36065	0.32996	0.17226
457	0.68023	0.37866	0.34396	0.18361
459	0.72896	0.41594	0.37284	0.20712
461	0.77637	0.45473	0.40363	0.23217
463	0.82033	0.49481	0.43703	0.25915
465	0.86162	0.53597	0.44976	0.28750

Table 4 $\ln g(\alpha)$ versus $\ln q$ curves of two types of probable mechanism functions when $0.1 < \alpha < 0.9$

T/K	Function No.	B	$-k$	$-r$
451	13	0.22302	1.05660	0.93994
	14	0.51929	1.02382	0.93786
452	13	0.27984	1.05425	0.94566
	14	0.56816	1.01901	0.94357
453	13	0.32976	1.04938	0.95030
	14	0.61005	1.01168	0.94820
454	13	0.37938	1.04486	0.95440
	14	0.65121	1.00457	0.95229
455	13	0.43114	1.04204	0.95829
	14	0.69403	0.99900	0.95616
456	13	0.48352	1.03935	0.96161
	14	0.73673	0.99331	0.95947
457	13	0.53135	1.03535	0.96443
	14	0.77472	0.98629	0.96228

results are listed in Table 4, they illustrate that the slope of No. 14 is the most adjacent to -1.00000 and correlation coefficient r is better. So we can determine that No. 14 mechanism function is the most probable one of the dehydration of $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$, with integral form $g(\alpha) = 1 - (1 - \alpha)^{1/2}$, belongs to the mechanism of phase boundary reaction, R_2 .

Calculation of pre-exponential factor A

The pre-exponential factor A were estimated from the intercept of the plots of Eq. 7 (the intercept, B , was shown in Table 2), inserting the most probable $g(\alpha)$ function determined (No. 14). The results showed that the range of

pre-exponential factor A was $0.8120 \times 10^7 - 2.6859 \times 10^7 \text{ s}^{-1}$, and average $A = 1.6915 \times 10^7 \text{ s}^{-1}$.

Determination of thermodynamic parameters of thermal decomposition reaction

Thermodynamic parameters (ΔS^\ddagger , ΔH^\ddagger , and ΔG^\ddagger) were calculated from Eqs. 12–14. The average values of the parameters were $\Delta S^\ddagger = -119.33 \text{ J mol}^{-1} \text{ K}^{-1}$, $\Delta H^\ddagger = 82.677 \text{ kJ mol}^{-1}$, and $\Delta G^\ddagger = 138.869 \text{ kJ mol}^{-1}$. As can be seen from the results, the values of ΔS^\ddagger for the dehydration step are negative. The positive values of ΔG^\ddagger at this step are due to the fact that dehydration of the crystal waters of $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ is not spontaneous at room temperature.

Conclusions

This study has successfully achieved a directly synthesis of single phase $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ via solid-state reaction at room temperature using $\text{LiH}_2\text{PO}_4 \cdot \text{H}_2\text{O}$, $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$, and Na_2CO_3 as raw materials. The thermal process of $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ in the range of ambient temperature to $800 \text{ }^\circ\text{C}$ is a two step process, which involves the dehydration of the one crystal water molecule at first, and then crystallization of LiZnPO_4 . The kinetics of the dehydration step of $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ was studied using iterative procedure, Ozawa–Flynn–Wall (OFW) method, and the Kissinger–Akahira–Sunose (KAS) method. Based on the iterative iso-conversional procedure, the average values of the activation energies associated with the thermal dehydration of $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$, was determined to be $86.59 \text{ kJ mol}^{-1}$. Dehydration of the crystal water molecule of $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ is single-step reaction mechanism. A method of multiple rate iso-temperature was used to define the most probable mechanism $g(\alpha)$ of the dehydration step. The dehydration step is contracting cylinder model ($g(\alpha) = 1 - (1 - \alpha)^{1/2}$) and is controlled by phase boundary reaction mechanism. The pre-exponential factor A is obtained on the basis of E_a and $g(\alpha)$. The thermodynamic parameters (ΔS^\ddagger , ΔH^\ddagger , and ΔG^\ddagger) of the dehydration reaction of $\alpha\text{-LiZnPO}_4 \cdot \text{H}_2\text{O}$ are obtained. These data will be important for further studies of the studied compound, and to solve various scientific and practical problems involving the participation of solid phases.

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